Material Balances:

It is more convenient to express balance equations in terms of mole ratios and on solute free basis:

- > Quantities of solvent are unchanged
- > Straight line operating lines



Nomenclature:

Gas Phase:

G:= Total gas flow rate

~ P5

mole / time/ unit cross sectional area
mole / time/ unit cross sectional area

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G_s:= Flow of insoluble gas (carrier)

y := solute mole fraction

Y := solute mole ratio = solute / carrier gas

 $\bar{p} := Partial pressure of solute$

$$Y = \frac{y G}{(1-y)G} = \frac{y}{(1-y)} = \frac{\overline{p}}{(p_t - \overline{p})} = \frac{\text{partial pressure of solute}}{\text{partial pressure of carrier}}$$

$$y = \frac{Y}{(1+Y)}$$

$$G_S = (1 - y) G = \frac{y}{y} G = \frac{Y}{1 + Y} \frac{1}{y} G$$

$$G_s = \frac{G}{(1+Y)}$$

Liquid Phase:

L:= Total liquid flow rate

mole / time/ unit cross sectional area

L_s:= Flow of liquid (carrier)

mole / time/ unit cross sectional area

x := solute mole fraction

X :=solute mole ratio = solute / solvent

$$X = \frac{x}{(1-x)}$$

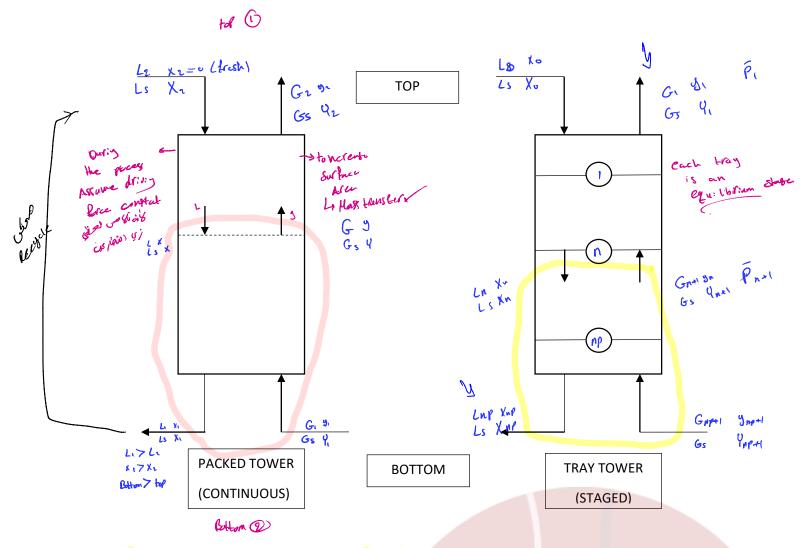
$$x = \frac{X}{(1+X)}$$

$$L_s = (1 - x) L$$

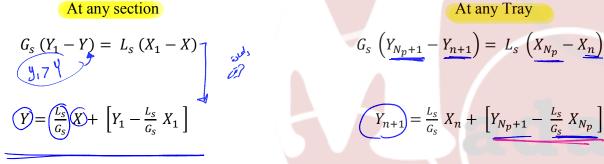
$$L_S = \frac{L}{(1+X)} \frac{1}{X} G$$

ask ;; belteve & recieve

Counter Current Flow (Absorption or Stripping)



Operating Lines (Solute Material Balances)



At any Tray

Notes:

- These are straight lines with slope = $\frac{L_s}{G_s}$ giving the relation between passing streams at any section or at any tray.
- For absorption (gas → liquid) carrier gas loses solute

 $Y_{bot} > Y_{top}$

 $X_{bot} > X_{top}$

For stripping (liquid → gas) carrier gas gains solute

 $Y_{bot} < Y_{top}$

 $X_{bot} < X_{top}$

For most purposes the pressure and temperature can be considered constant inside the column

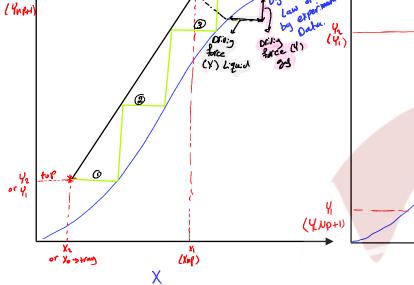
The operating lines can be plotted together with equilibrium data on XY diagram.

y(flxi)

Shope = $\left(\frac{Gs}{Gs}\right)$

Absorption





(No)

Stripping

Concentration gradient in direction of mass transfer

and
$$\gamma_1 \longrightarrow \gamma_2$$