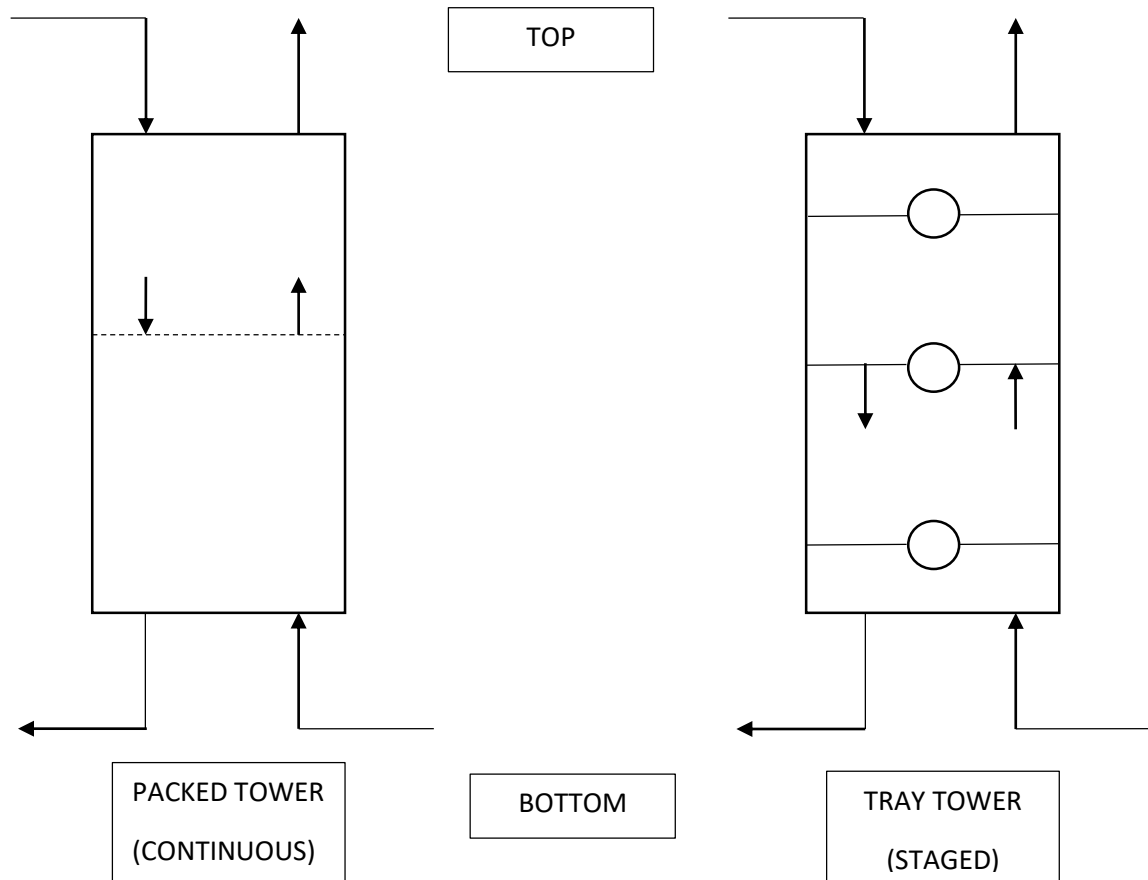


### Liquid Phase:

## Counter Current Flow (Absorption or Stripping)



## Operating Lines (Solute Material Balances)

At any section

$$G_s (Y_1 - Y) = L_s (X_1 - X)$$

$$Y = \frac{L_s}{G_s} X + \left[ Y_1 - \frac{L_s}{G_s} X_1 \right]$$

At any Tray

$$G_s (Y_{N_p+1} - Y_{n+1}) = L_s (X_{N_p} - X_n)$$

$$Y_{n+1} = \frac{L_s}{G_s} X_n + \left[ Y_{N_p+1} - \frac{L_s}{G_s} X_{N_p} \right]$$

**Notes:**

- These are straight lines with slope  $= \frac{L_s}{G_s}$  giving the relation between passing streams at any section or at any tray.
- For absorption (gas  $\rightarrow$  liquid) carrier gas loses solute

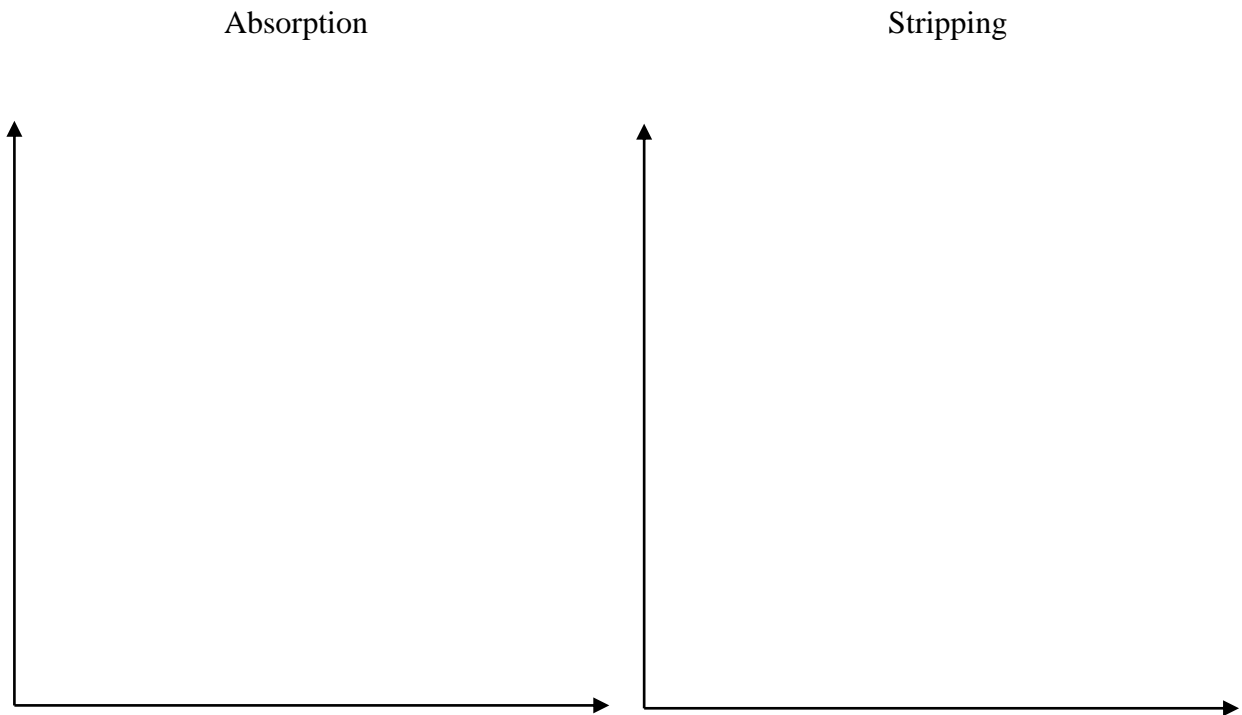
$$Y_{bot} > Y_{top} \quad ; \quad X_{bot} > X_{top}$$

- For stripping (liquid  $\rightarrow$  gas) carrier gas gains solute

$$Y_{bot} < Y_{top} \quad ; \quad X_{bot} < X_{top}$$

- For most purposes the pressure and temperature can be considered constant inside the column

The operating lines can be plotted together with equilibrium data on XY diagram.

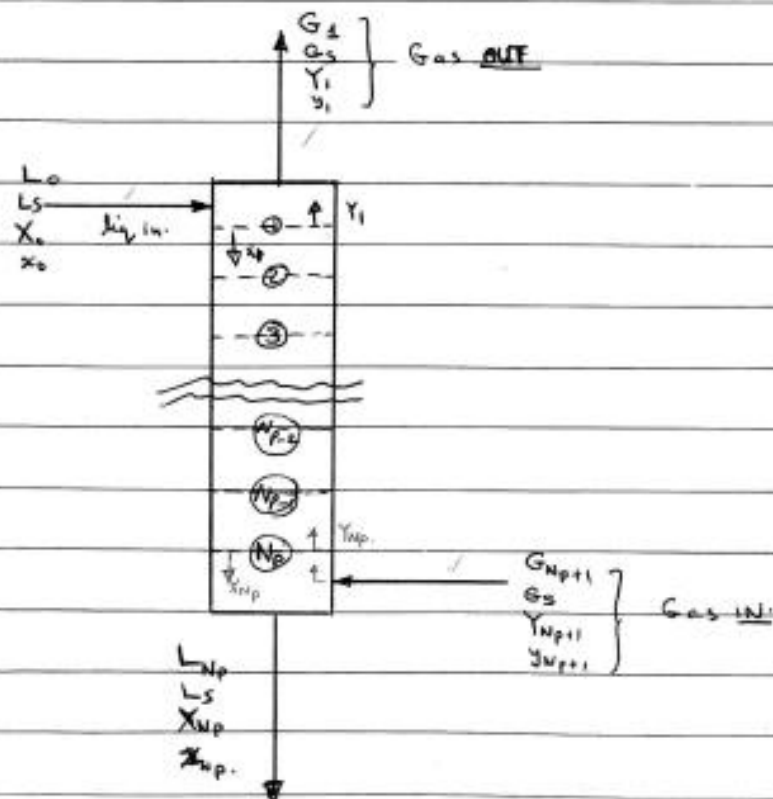
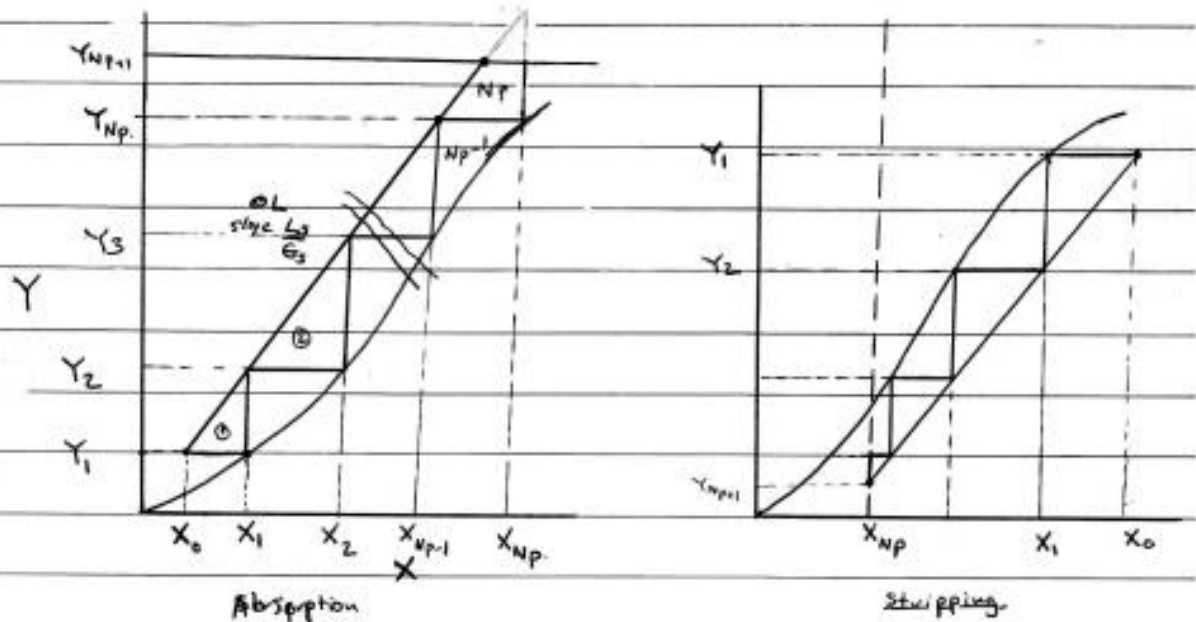


Concentration gradient in direction of mass transfer

## TRAY TOWERS: ONE COMPONENT TRANSFERRED:

(ABSORBERS OR STRIPPERS)

Number of theoretical plates <sup>can be</sup> determined graphically.



Absorption  $Y_{Np+1}, Y_1$  and  $X_0$  are fixed

Stripping  $X_0, X_{Np}$  and  $Y_{Np+1}$  are fixed