Dilute solutions obeying Henry's law:

Tray Towers:

Dalton's law: $p = y p_t$

Henry's law: $p = \mathcal{H} x$ (Raoult's law: $p = p^s x$)

$$y = \frac{\mathcal{H}}{p_t} x$$

$$y = m x y = \frac{p}{p_t} x$$

Where m is a constant

This is a straight line equation using mole fractions

For dilute solutions

$$y \cong Y$$
 and $x \cong X$
 $G \cong G_S$ $L \cong L_S$

: any concentration unit will give straight lines: operating and equilibrium

In these cases the number of theoretical plates can be determined using the Kremser equations

	Absorption	Stripping
<i>A</i> ≠ 1	$N_{p} = \frac{\left[\frac{N_{N_{p}+1} - mx_{o}}{y_{1} - mx_{o}} \left(1 - \frac{1}{A}\right) + \frac{1}{A}\right]}{\log A}$	$= \frac{\log \left[\frac{x_o - N_{N_p+1}/m}{y_1 - N_{N_p+1}/m} \left(1 - \frac{1}{S} \right) + \frac{1}{S} \right]}{\log S}$
A = 1	$N_p = \frac{y_{N_p + 1} - y_1}{y_1 - mx_o}$	$N_p = \frac{x_o - x_{N_p}}{x_{N_p} - \frac{y_{N_p+1}}{m}}$

$$A = L/_{mG}$$
, and $S = {^{mG}}/_{L}$

Notes:

- These relations can also be used with mole ratios since $y \cong Y$ and $x \cong X$
- If A top is not the same as A bottom, a geometric average can be used $A_{average} = \sqrt[2]{A_{top} \cdot A_{bottom}}$

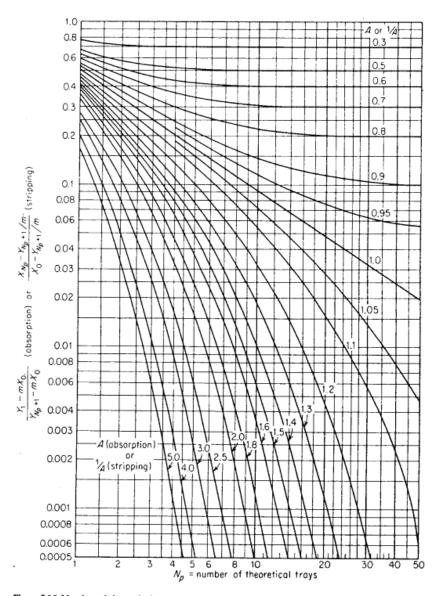


Figure 5.16 Number of theoretical stages for countercurrent cascades, with Henry's law equilibrium and constant absorption or stripping factors. [After Hachmuth and Vance, Chem. Eng. Prog., 48, 523, 570, 617 (1952).]

Packed Towers:

The Kremser type equations for packed towers may be used:

$$y = m x$$

For absorbers:

$$N_{tOG} = \frac{ln\left[\frac{y_1 - mx_2}{y_2 - mx_2}\right]\left(1 - \frac{1}{A}\right) + A}{1 - \frac{1}{A}}$$

A =absorption factor =
$$\frac{L}{mG}$$

For strippers:

$$N_{tOL} = \frac{ln\left[\frac{x_2 - y_1/m}{x_1 - y_1/m}\right](1 - A) + A}{1 - \frac{1}{A}}$$

Relationship between N_{tOG} and N_p :

$$N_{tOG} = \frac{1}{1 - \frac{1}{A}} \ln A \ N_p$$
 $A = 1.25$
 $N_{tOG} = 1.116 \ N_p$
 $N_{tOG} = 1.386 \ N_p$

For Strippers

$$N_{tOL} = \frac{\ln(S)}{1 - A} N_p$$