

**University of Jordan**  
**Chemical Engineering Department**  
**Chemical Engineering Thermodynamics (1) – 905322**



**Lecture 17: Refrigeration, Liquefaction, and Mechanical Explosions**

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**Outline**

- Refrigeration
  - Importance of refrigeration
  - Refrigerators and Refrigerants
  - Analysis
- Liquefaction
  - Simple Liquefaction
  - Linde Liquefactions
- Mechanical Explosions
  - TNT Equivalents
  - Vapor Phase Explosions
  - BELEVE Explosions



# Importance of Refrigeration

- Air conditioning (AC).
- Treatment, transportation and preservation of foods and beverages.
- Dehydration of gases.
- Production of ice.
- Air distillation.
- Lubricating-oil purification.
- Low temperature reactions.
- Separation of volatile hydrocarbons.
- Biomedical.

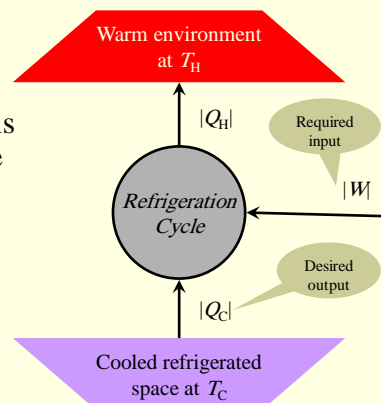


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# Refrigeration Terminology

- A **refrigerator** is a device which removes heat from a low temperature region to a high temperature region.
- The **objective of a refrigerator** is to maintain the refrigerated space at low temperature by discarding and/or removing heat from it.
- A **refrigerant** is the working fluid used in the refrigeration cycle.



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# Refrigeration Efficiency

- A **ton of refrigeration** is the equivalent of heat removal rate at 211 kJ/min (200 Btu/min).
- Efficiency in refrigeration is defined in terms of coefficient of performance COP.

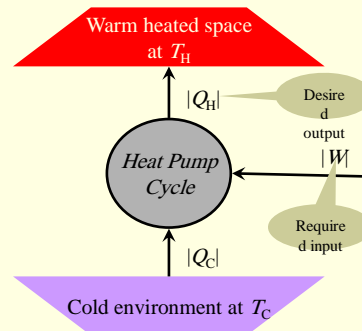
$$\text{COP}_R = \frac{\text{Desired output}}{\text{Required input}} \geq 0$$

$$\text{COP}_R = \frac{|Q_C|}{|W|} = \frac{1}{|Q_H|/|Q_C| - 1} = \frac{1}{T_H/T_C - 1} \geq 0 \quad (1)$$



# Carnot Heat Pump

- A device that transfers heat from a **low**  $T$  medium to a high  $T$  medium.
- The objective of a heat pump is to **supply heat into the warmer space**.
- Efficiency is defined in terms of coefficient of performance COP.

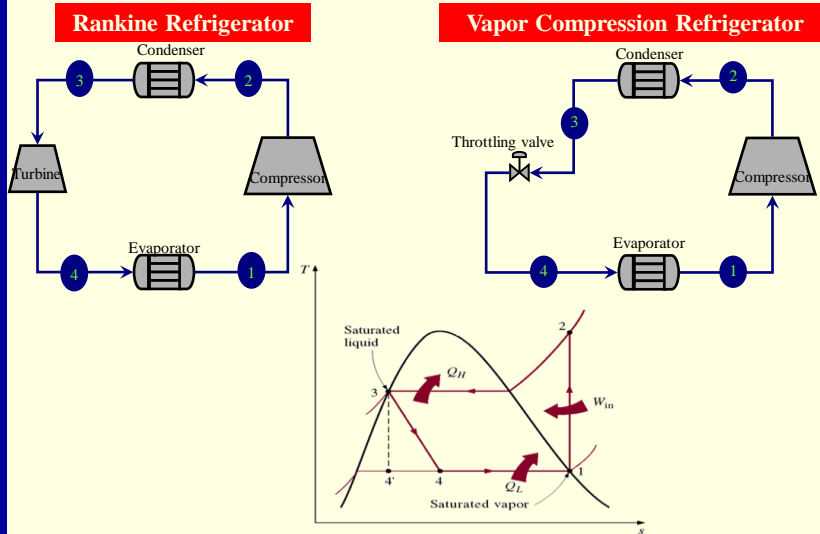


$$\text{COP}_{HP} = \frac{\text{Desired output}}{\text{Required input}} \geq 1$$

$$\text{COP}_{HP} = \frac{|Q_H|}{|Q_H| - |Q_C|} = \frac{1}{1 - |Q_C|/|Q_H|} = \frac{1}{1 - T_C/T_H} \geq 1 \quad (2)$$



# Rankine & Vapor Compression Cycles

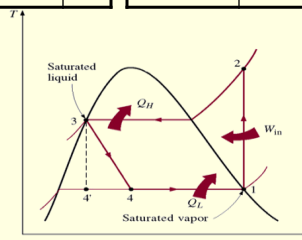


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## Rankine & Vapor Compression Cycles II

Rankine Refrigerator				Vapor Compression Refrigerator			
Turbine	Sat. L to V-L (3→4)	Isentropic	$W_T$	Throttling valve	Sat. L to V-L	Isenthalpic	0
Evaporator	V-L to Sat. V	Isothermal-Isobaric	$Q_H$	Evaporator	V-L to Sat. V	Isothermal-Isobaric	$Q_H$
Compressor	Sat. V to Superheated V.	Isentropic	$W_C$	Compressor	Sat. V to Superheated V.	Isentropic	$W_C$
Condenser	Superheated V. to Sat. L.	Isobaric	$Q_C$	Condenser	Superheated V. to Sat. L.	Isobaric	$Q_C$



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# Refrigeration Efficiency

- COP for the Rankine cycle

$$\text{COP}_R = \frac{Q_{\text{Evaporator}}}{W_{\text{Compressor}} + W_{\text{Turbine}}} = \left| \frac{H_1 - H_4}{(H_2 - H_1) + (H_4 - H_3)} \right| \quad (3)$$

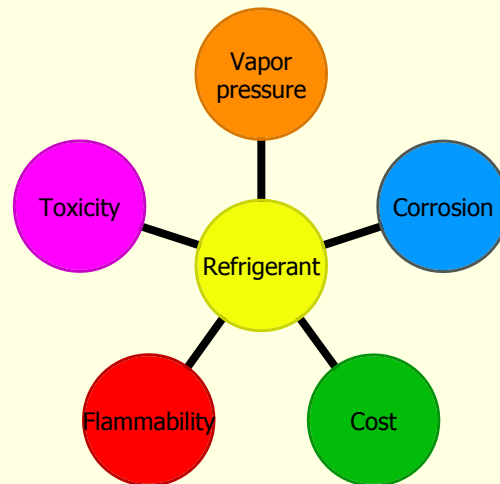
- COP for the ideal vapor compression cycle

$$\text{COP}_R = \frac{Q_{\text{Evaporator}}}{W_{\text{Compressor}}} = \left| \frac{H_1 - H_4}{H_2 - H_1} \right| \quad (3')$$

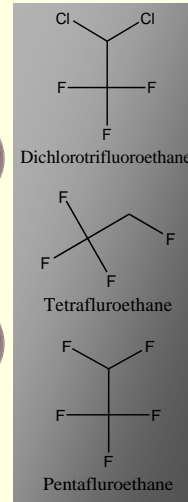
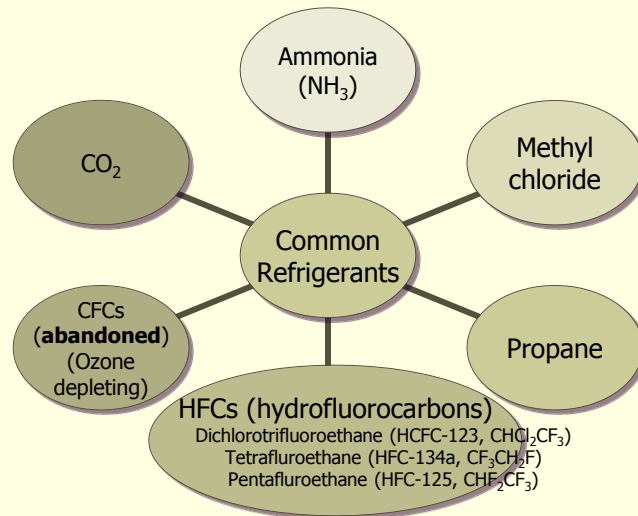


# Choice of Refrigerant

- The COP of the Carnot refrigerator is independent of the type of refrigerant used.
  - Not true for real refrigerators due to inherent irreversibilities.



# Common Refrigerants



# Liquefaction

- Liquefaction is the process by which gases are liquefied.
- Important in many areas e.g., Liquefied Natural Gas (LNG), and refrigerant gases.
- Two different approaches for liquefaction:
  - Cool the gas down to below its boiling-point temperature at the desired pressure
    - not practical due to cooling requirements.
  - **Compress** the gas to high  $P \rightarrow$  **cool** at the same  $P \rightarrow$  **expand** to low  $P$  and  $T$  using **Joule-Thompson** expansion.

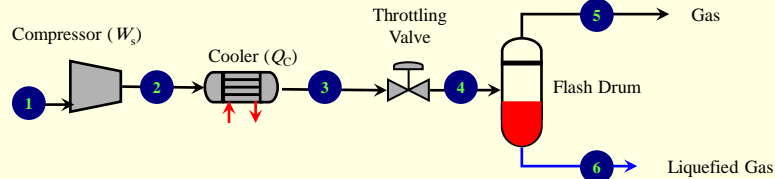


$$\eta_{\text{Liquefaction}} = \frac{\text{Amount of liquefied gas produced}}{\text{Work done in the compressor}}$$

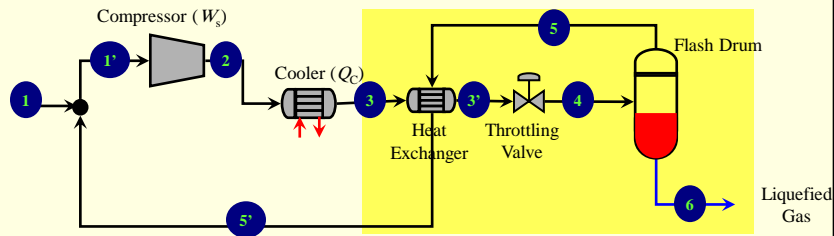


# Simple and Linde Liquefaction

## a) Simple liquefaction process without recycle.



## b) Linde liquefaction process with recycle.



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# Linde Process Calculations

- Use the **heat exchanger, throttle valve** and **flash drum** as a system

- Mass balance

$$M_3 = M_{5'} + M_6$$

- Energy balance

$$M_3 \underline{H}_3 = M_{5'} \underline{H}_{5'} + M_6 \underline{H}_6$$

- Solve for the liquid fraction  $x$ .

- Base the flow on 1 kg to the compressor

$$M_{1'} = 1; \quad M_{5'} = 1 - x; \quad M_1 = x$$

- Find the enthalpy at the compressor inlet

$$\underline{H}_{1'} = M_{5'} \underline{H}_{5'} + M_1 \underline{H}_1$$

- Find compressor work using the isentropic conditions (multistage & intercooling?)

$$W = \underline{H}_2 - \underline{H}_{1'}$$

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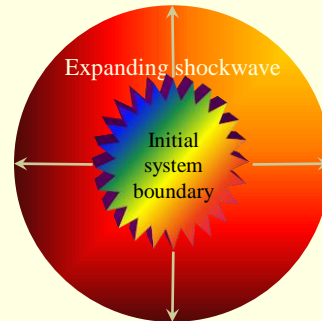
# Mechanical Explosions

## ■ Explosions that occur without reaction.

- Bursting of an overpressurized tank.
- Rapid depressurization of a hot liquid that leads to partial flashing.

## ■ Explosions

- **Very rapid** that there is no heat or mass transfer to/from the surroundings to the exploding material.
- The exploding material undergoes a **rapid (and uniform) expansion**, pushing away the surrounding air.



shockwave speed

$M < 1$  Deflagration

$M = 1$  Explosion

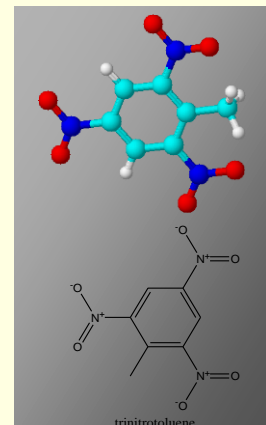
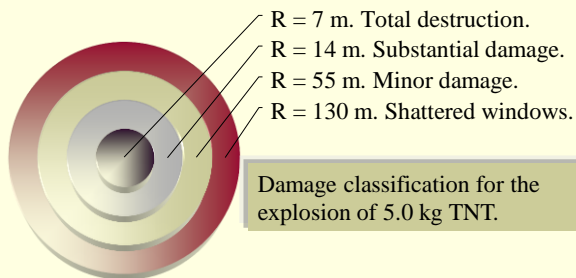
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# Explosion Equivalents

## ■ Trinitrotoluene (TNT) is the standard to measure explosions against.

- Blast energy = 4600 kJ/kg.



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# Vapor-Phase Explosions

- Assumptions: closed system, isentropic

Energy balance  $W = M[\hat{U}(T_f, P = \text{ambient}) - \hat{U}(T_i, P_i)]$  (4)

Entropy balance  $\hat{S}(T_f, P = \text{ambient}) = \hat{S}(T_i, P_i)$  (5)

- Ideal gas case ( $V_S$  is the initial system volume)

$$T_f = T_i \left( \frac{P = \text{ambient}}{P_i} \right)^{R/C_p^*} \quad (6)$$

$$-W = \frac{P_i V_S}{\gamma - 1} \left[ 1 - \left( \frac{P = \text{ambient}}{P_i} \right)^{(\gamma-1)/\gamma} \right] \quad (7)$$



# Boiling Liquid Evaporating Vapor Explosions (BLEVEs)

- A compressed liquid or Liquid-Vapor mixture undergoing sudden depressurization may partially or completely vaporize.

Energy balance  $W = M[X_f \hat{U}^V(T_f, P = \text{ambient}) + (1 - X_f) \hat{U}^L(T_f, P = \text{ambient})] - M[X_i \hat{U}^V(T_i, P_i) + (1 - X_i) \hat{U}^L(T_i, P_i)]$  (8)

Entropy balance  $X_f \hat{S}^V(T_f, P = \text{ambient}) + (1 - X_f) \hat{S}^L(T_f, P = \text{ambient}) = X_i \hat{S}^V(T_i, P_i) + (1 - X_i) \hat{S}^L(T_i, P_i)$  (9)



# Simplified BELEVE Analysis

- Estimate the vapor fraction and the energy released from only knowledge of specific heat of liquid and the latent heat of vaporization.

Energy released

$$-W = M \left[ C_p^L (T_i - T_b) - X_f \left( \Delta \hat{H}^{\text{vap}} - \frac{RT}{MW} \right) \right] \quad (10)$$

Final vapor fraction

$$X_f = 1 - \exp \left[ \frac{C_p^L}{\Delta \hat{H}^{\text{vap}}} (T_b - T_i) \right] \quad (11)$$

