## **Bioreactor and Microbial Growth**

# **Bioreactor**

- A reactor that sustains and supports life for cells and tissue cultures.
- Cellular reactions include:
  - Transformation of chemical energy
  - Construction, breakdown, and digestion of cellular components
- Enzymatic reactions are involved in the growth of microorganisms (microbial growth)
- Monod equation:
  - Describes the growth law for a number of bacteria
  - Similar to Michaelis-Menten equation

# **Bioconversion Advantages**

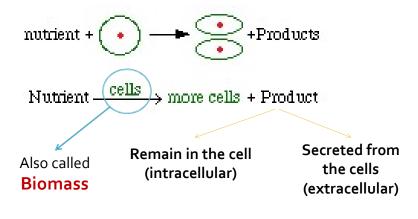
- Mild reaction conditions
- High yield
- Organisms contain several enzymes that can catalyze successive steps in a reaction
- Enzymes act as stereospecific catalyst

## **Schematic of Cell**



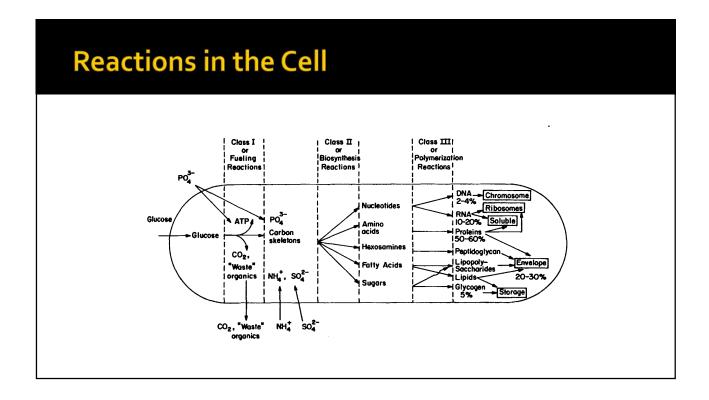
- Cell wall: protect the cell from external influence
- Cell membrane: provides for selective transport of material into and out of the cell
- Cytoplasm: contains the ribosomes that contain ribonucleic acid (RNA)
- Nuclear region: contains deoxyribonucleic acid (DNA) which provides genetic information for the production of proteins and other cellular substances and structures.

# Biosynthesis



## **Reactions in the Cell**

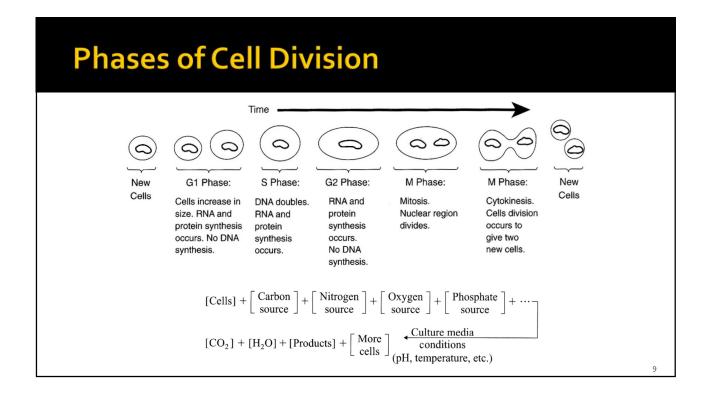
- All take place simultaneously and are classified as either:
  - Nutrient degrading (fueling reactions)
  - II. Synthesis of small molecules (amino acids)
  - III. Synthesis of large molecules (RNA, DNA)
- Autocatalytic reaction: the rate of growth is proportional to cell concentration

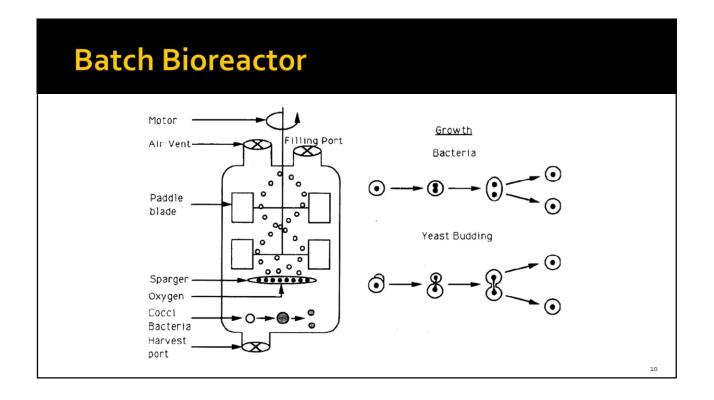


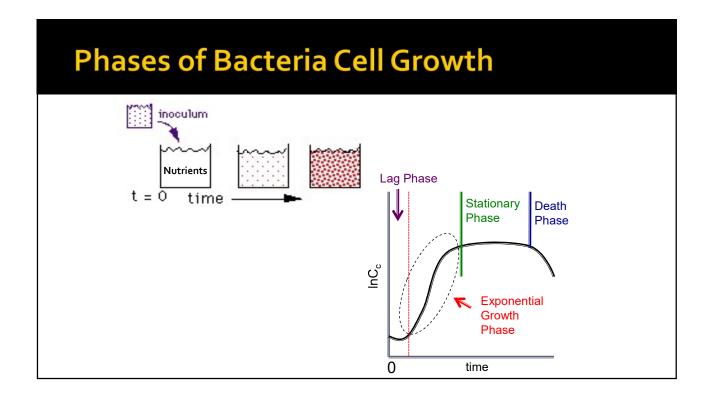
# **Reactions in the Cell**

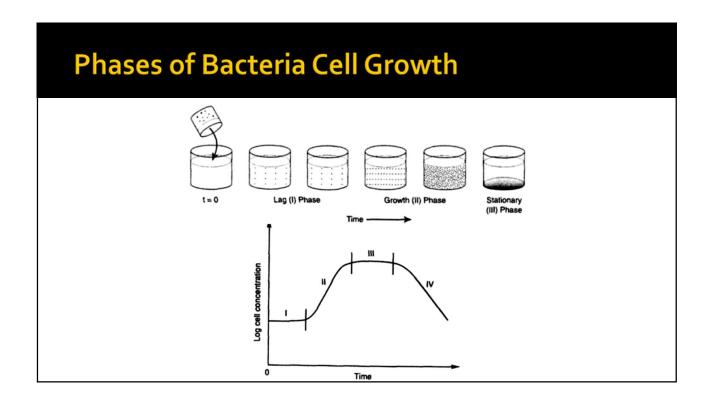
 ATP also transfers the energy it releases when it loses phosphonate group to form adenosine diphosphate (ADP)

$$ATP + H_2O \rightarrow ADT + P + H_2O + Energy$$









# **Rate Laws**

The rate of microbial growth is characterized by the net specific growth rate,  $\mu_{net}$  (1/time), defined as

$$\mu_{\text{net}} = \frac{1}{X} \frac{dX}{dt}$$

 $\mu_{\rm net} \equiv \frac{1}{X} \frac{dX}{dt}$  X: cell mass concentration

t: time

## **Rate Laws**

$$\mu_{\text{net}} \equiv \frac{1}{X} \frac{dX}{dt}$$

$$\mu_{\text{net}} = \mu_g - k_d$$

 $\mu_g$ : Gross specific growth rate

 $k_d$ : Rate of loss of cell mass due to cell death or

endogenous metabolism

# **Rate Laws**

$$\mu_{\rm R} \equiv \frac{1}{N} \frac{dN}{dt} \equiv \text{net specific replication rate}$$

N: Cell number concentration (cell number /L)

$$\mu_{R} = \mu'_{R} - k_{d}$$

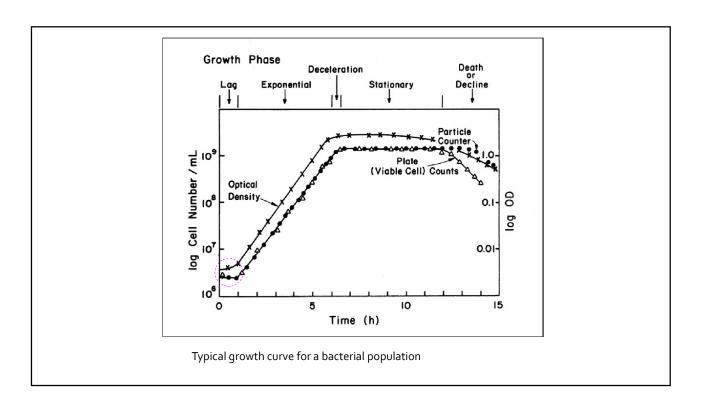
 $\mu_R'$  : Gross specific replication rate (1/time)

 $k_d$ : Rate of cell death (1/time)

When cell death is unimportant,  $\mu_R = \mu_R'$ 

## **Growth Kinetics**

- In batch culture:
  - lag phase
  - logarithmic or exponential growth phase
  - deceleration phase
  - stationary phase
  - death phase

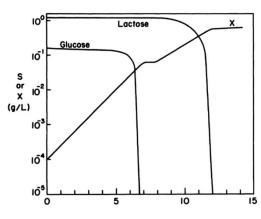


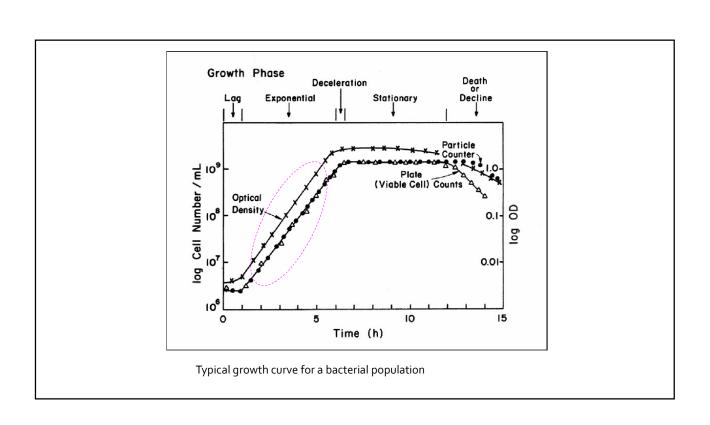
### Lag phase

- A period of adaptation for the cells to their new environment
  - New enzymes are synthesized.
  - A slight increase in cell mass and volume, but no increase in cell number
  - Prolonged by low inoculum volume, poor inoculum condition (high % of dead cells), age of inoculum, nutrient-poor medium
  - Multiple lag phases (*diauxic growth*): medium contains more than one carbon source

# Diauxic growth curve for *E. coli* on Glucose and Lactose

- At 2 h after inoculation, cells are growing rapidly, glucose is being consumed, and lactose is not being utilized.
- At 7 h, cell mass accumulation is zero.
   All the glucose has been consumed.
- At 10 h the culture is growing and lactose is being consumed, but the rate of growth (cell mass accumulation) is less than at 2 h.





## **Exponential growth phase**

- In this phase, the cells have adjusted to their new environment and multiply rapidly (exponentially)
  - Balanced growth all components of a cell grow at the same rate.
  - Growth rate is independent of nutrient concentration, as nutrients are in excess.

## **Batch Growth Kinetics**

## **Exponential growth phase**

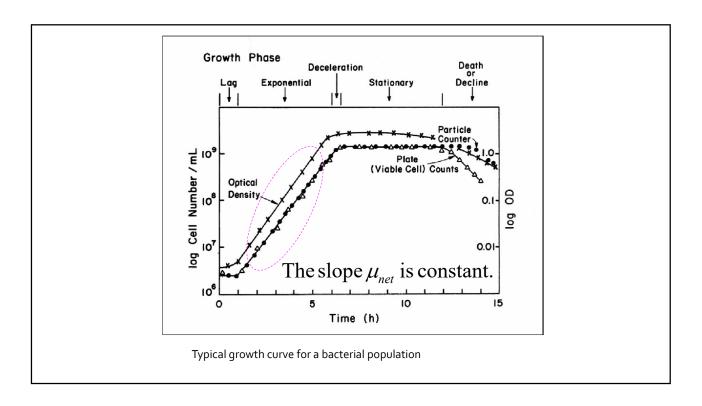
The balance of cell mass in a batch culture gives:

$$\frac{dX}{dt} = \mu_{net}X, \ X = X_0 \ at \ t = 0$$

Integration of the above equation yields:

$$\ln \frac{X}{X_0} = \mu_{net}t$$
, or  $X = X_0e^{\mu_{net}t}$ 

X and  $X_0$  are cell concentrations at time t and t=0



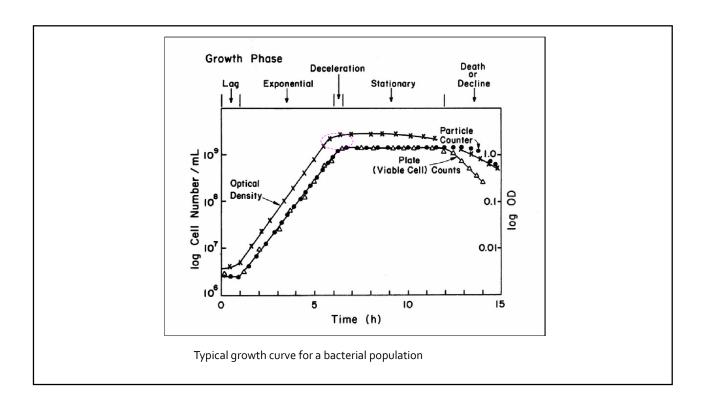
## **Exponential growth phase**

$$\mu_{net} = \mu_{R} = \mu_{m}$$

 $\mu_m$  is the maximum specific growth rate (1/time)

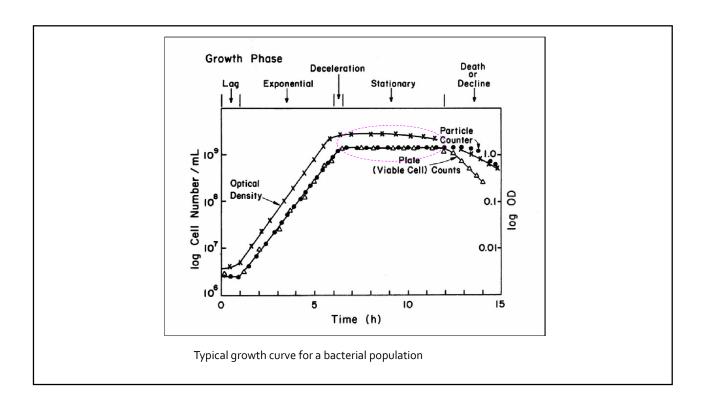
• **Doubling time of cell mass (** $au_d$ ): the time required to double the microbial mass:

$$\tau_d = \frac{\ln X / X_0}{\mu_{\text{net}}} = \frac{\ln 2}{\mu_{\text{net}}} = \frac{0.693}{\mu_{\text{net}}}$$



## **Deceleration growth phase**

- Very short phase, during which growth decelerates due to either:
  - Depletion of one or more essential nutrients
  - The accumulation of toxic by-products of growth (e.g. Ethanol in yeast fermentations)
  - Period of unbalanced growth: Cells undergo internal restructuring to increase their chances of survival



## **Stationary Phase:**

- With the exhaustion of nutrients (S ≈ 0) and build-up of waste and secondary metabolic products
  - Net growth rate = 0 (no cell division).
  - growth rate = death rate
  - Cells are still metabolically active and produce secondary metabolites.
- **Primary metabolites** are growth-related: ethanol by *S. cerevisαe*.
- Secondary metabolites are non-growth-related: antibiotics.

### **Stationary phase**

- One or more of the following phenomena may take place:
  - Total cell mass concentration may stay constant, but the number of viable cells may decrease.
  - 2. Cell lysis may occur and viable cell mass may drop. A second growth phase may occur and cells may grow on lysis products of lysed cells (<u>cryptic growth</u>).
  - 3. Cells may not be growing but may have active metabolism to produce secondary metabolites.

## **Batch Growth Kinetics**

## **Stationary phase**

- Endogenous metabolism occurs by catabolizing cellular reserves for new building blocks and energy-producing monomer (maintenance energy).
- The rate describing the conversion of cell mass into maintenance energy or the loss of cell mass due to cell lysis:

$$\frac{dX}{dt} = -k_d X$$

 $k_d$  is the rate constant for endogenous metabolism

### **Death Phase:**

- The living organism population decreases with time, due to a lack of nutrients and accumulation of toxic metabolic by-products.
- The rate of death usually follows first order kinetics:

$$\frac{dN}{dt} = -k'_{d} N \qquad or \qquad N = N_{S} e^{-k'_{d}t}$$

 $N_{S}$  is the concentration of cells at the end of the stationary phase  $k'_{d}$  is the first - order death rate constant

## **Batch Growth Kinetics**

 Yield coefficients: defined based on the amount of consumption of another material.

Growth yield: 
$$Y_{X/S} \equiv -\frac{\Delta X}{\Delta S}$$

Product yield: 
$$Y_{P/S} \equiv -\frac{\Delta P}{\Delta S}$$

Growth yield based on consumption of oxygen:

$$Y_{X/O_2} \equiv -\frac{\Delta X}{\Delta O_2}$$

$$\Delta S = \Delta S_{\substack{\text{assimilation}\\ \text{into biomass}}} + \Delta S_{\substack{\text{assimilation}\\ \text{into an}\\ \text{extracellular}\\ \text{product}}} + \Delta S_{\substack{\text{growth energy}\\ \text{energy}}} + \Delta S_{\substack{\text{maintenance}\\ \text{energy}}}$$

- Yield coefficients: defined based on the amount of consumption of another material.
- For most bacteria and yeast:

$$Y_{X/S} = 0.4 - 0.6 \text{ g/g glucose}$$

$$Y_{X/O_2} = 0.9 - 1.4 g/g O_2$$

 At the end of the batch growth period, the measured yields are apparent as endogenous metabolism occurring, K<sub>d</sub> > 0, which changes the metabolic pathways of the substrate.

$$Y_{X/S}^{M} > Y_{X/S}^{App}$$

# How Environmental Conditions Affect Growth Kinetics

- Patterns of microbial growth and product formation are influenced by environmental conditions such as
  - Temperature
  - pH
  - Dissolved-oxygen concentration

#### **Temperature**

- An important factor affecting the performance of cells
- According to their temperature optima, organisms can be classified in three groups:
  - 1. Psychrophiles  $(T_{opt} < 20$ °C)
  - 2. Mesophiles ( $20^{\circ} < T_{opt} < 50^{\circ}C$ )
  - Thermophiles (T<sub>opt</sub> > 50°C)
- As the temperature is increased toward optimal growth temperature, the growth rate approximately doubles for every 10°C increase in temperature.
- Above the optimal temperature range, the growth rate decreases and thermal death may occur.

# How Environmental Conditions Affect Growth Kinetics

## **Temperature**

The net specific replication rate can be expressed by the following equation for temperature above optimal level:

$$\frac{dN}{dt} = (\mu_R' - k_d')N$$

$$\mu_R' = Ae^{-E_a/RT}, \quad k_d' = A'e^{-E_d/RT}$$

 At high temperatures, the thermal death rate exceeds the growth rate, which causes a net decrease in the concentration of viable cells.

### **Temperature**

- Temperature also affects:
  - product formation
    - the temperature optimum for growth and product formation may be different
  - yield coefficient
  - rate-limiting step in a fermentation process
    - At high temperatures, the rate of bioreaction might become higher than the diffusion rate, and diffusion would then become the ratelimiting step (for example, in an immobilized cell system)

# How Environmental Conditions Affect Growth Kinetics

### Hydrogen-ion concentration (pH)

- pH affects the activity of enzymes and therefore the microbial growth rate
- The optimal pH for growth may be different from that for product formation.
- Different organisms have different pH optima:
  - for many bacteria: pH = 3 to 8
  - for yeast: pH = 3 to 6
  - for molds: pH = 3 to 7
  - for plant cells: pH = 5 to 6
  - for animal cells: pH = 6.5 to 7.5

### Hydrogen-ion concentration (pH)

- Many organisms have mechanisms to maintain intracellular pH at a relatively constant level in the presence of fluctuations in environmental pH.
- When pH differs from the optimal value, the maintenance-energy requirements increase.
- One consequence of different pH optima is that the pH of the medium can be used to select one organism over another.

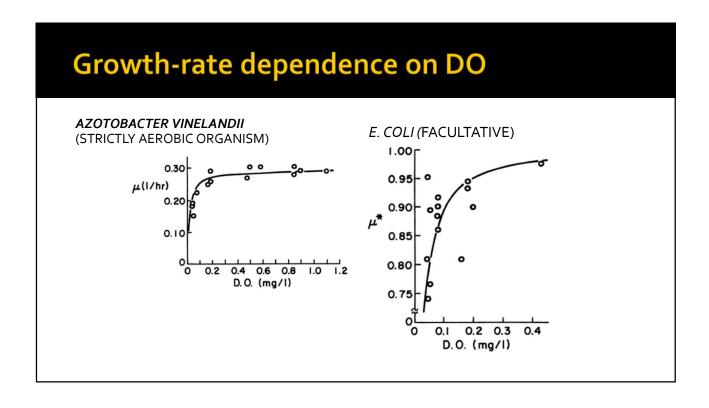
# How Environmental Conditions Affect Growth Kinetics

### Dissolved oxygen (DO)

- Aerobic fermentation requires oxygen
- Oxygen gas is sparingly soluble in water
- If DO is below a critical oxygen concentration, growth or respiration approaches a first-order rate dependence on the DO concentration.
- Above a critical oxygen concentration, growth rate becomes independent of DO concentration.
- Oxygen is a growth-rate-limiting factor when the DO level is below the *critical DO concentration*.

## Dissolved oxygen (DO)

- Critical oxygen concentration for
  - bacteria and yeast: 5%-10% of the saturated DO
  - mold: 10%-50% of the saturated DO
- The saturated DO in aqueous solution is 7 ppm at 250C and 1 atm.
- Factors affecting the saturation value
  - the presence of dissolved salts and organics can alter the saturation value
  - increasingly high temperatures decrease the saturation value



#### **Environmental Conditions**

# Dissolved oxygen (DO)

- Oxygen is usually introduced to fermentation broth by sparging air through the broth.
- Oxygen transfer from gas bubbles to cells is usually limited by oxygen transfer through the liquid film surrounding the gas bubbles.
- The rate of oxygen transfer from the gas to liquid phase (OTR) is given by

OTR = 
$$N_{O_2} = k_L a (C*-C_L)$$

k<sub>1</sub>: the oxygen transfer coefficient (cm/h)

a: the gas-liquid interfacial area (cm²/cm³)

k<sub>1</sub> a: the volumetric oxygen transfer coefficient (h-1)

C\*: saturated DO concentration (mg/l);

C<sub>L</sub>: the actual DO concentration (mg/l);

 $N_{O_2}$ : the rate of oxygen transfer (mg  $O_2/l-h$ )

#### **Environmental Conditions**

# Dissolved oxygen (DO)

• Rate of oxygen uptake (OUR) is oxygen consumption rate by microbes. If the maintenance requirement of O2 is negligible compared to growth, then

$$OUR = q_{o_2} X = \frac{\mu_g X}{Y_{X/O_2}} \text{ (mg O}_2/\text{h)}$$

 $q_{o_2}$  is the specific rate of  $O_2$  consumption (mg  $O_2$ /g cells-h)

 When oxygen transfer is the rate-limiting step, at steady state, the rate of oxygen consumption is equal to the rate of oxygen transfer.

$$\frac{\mu_g X}{Y_{X/O_2}} = k_L a(C^* - C_L)$$

$$OR \frac{dX}{dt} = Y_{X/O_2} k_L a(C^* - C_L)$$

Sufficient oxygen supply: OTR ≥ OUR

#### **Environmental Conditions**

# Dissolved oxygen (DO)

#### Question:

Oxygen is to be supplied for yeast production. If oxygen uptake rate (OUR) is 15 g/l medium-h for a required yeast growth, and the oxygen transfer rate (OTR) is 10 g/l medium-h. Is such oxygen transfer rate sufficient to maintain the required yeast growth? If the required growth has to be maintained, how to improve the oxygen transfer rate?

#### Answers:

OUR = 15g/l medium-h > OTR = 10 g/l medium-h

insufficient oxygen supply rate

Oxygen transfer rate is limiting

Increase (
$$k_{\rm L}a$$
) so that  $\frac{\mu_g X}{Y_{X/O_2}} = k_L a (C*-C_L)$ 

### **Environmental Conditions**

# Ionic Strength (I)

- Ionic strength of a medium (I) affects
  - the transport of certain nutrients in and out of cells
  - the metabolic functions of cells,
  - the solubility of certain nutrients (dissolved oxygen and minerals)

$$I = \frac{1}{2} \Sigma C_i Z_i^2$$

C: the concentration of an ion

Z: its charge

## **Environmental Conditions Effect**

- **High substrate concentration**: substrate inhibition
- Substrate inhibition can be overcome by intermittent addition of the substrate to the medium.

# Exercise (P6.2)

The growth of a microbial population is a function of pH and is given by the following equation:

$$\mu_{g} = \frac{1}{X} \cdot \frac{dX}{dt} = \frac{\mu_{m}S}{K_{s} \left(1 + \frac{H^{+}}{k_{1}}\right) + S}$$

- A. With a given set of experimental data (X and S versus t), describe how you would determine the constants  $\mu_m$ ,  $K_S$ , and  $k_1$ .
- B. How would the double-reciprocal plot  $1/\mu_g$  versus 1/S change with pH (or H<sup>+</sup> concentration)?

#### **Batch Growth**

## Heat generation by microbial growth

- About 40% to 50% of the energy stored in a carbon and energy source is converted to biological energy (ATP) during aerobic metabolism, and the rest of the energy is released as heat.
- For actively growing cells, the maintenance requirement is low, and <u>heat evolution</u> is directly related to <u>growth</u>.

### **Batch Growth**

## Heat generation by microbial growth

• The heat of combustion of the <u>substrate</u> is equal to the sum of the metabolic heat and the heat of combustion of the cellular material.

$$\frac{\Delta H_S}{Y_{X/S}} = \Delta H_C + \frac{1}{Y_H}$$

 $\Delta H_{S}$ : the heat of combustion of the substrate (kJ/g substrate)

 $Y_{_{x/s}}\,\,$  : the cell mass yield per substrate consumption (g cell/g substrate)

 $\Delta H_{\,c}\,$  : the heat of combustion of cells (kJ/g cells)

 $\frac{1}{Y_H}$  : the metabolic heat evolved per gram of cell mass produced (kJ/g cells)

#### **Batch Growth**

## Heat generation by microbial growth

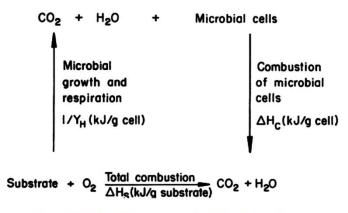


Figure 6.10. Heat balance on microbial utilization of substrate.

### **Batch Growth**

# Heat generation by microbial growth

Re-arrange the above equation:

$$\frac{1}{Y_H} = \frac{\Delta H_S}{Y_{X/S}} - \Delta H_C$$

The higher degree of oxidation of the substrate has lower amounts of heat released:

1/Y<sub>H</sub>

Glucose: 2.38 kcal/g cell produced ethanol: 5.55 kcal/g cell produced Methanol: 8.33 kcal/g cell produced Methane: 16.34kcal/g cell produced

#### **Batch Growth**

## Heat generation by microbial growth

$$\frac{1}{Y_H} = \frac{\Delta H_S}{Y_{X/S}} - \Delta H_C$$

The total rate of heat evolution in a batch fermentation  $Q_{\mathsf{GR}}(kJ/h)$  is

$$Q_{_{GR}} = V_L \mu_{net} X \frac{1}{Y_{_{_{\! H}}}}$$

 $X: \text{cell mass concentration (g/L);} \quad V_L: \text{liquid volume (L)}$ 

### **Batch Growth**

## Heat generation by microbial growth

• In aerobic fermentations, the rate of metabolic heat evolution  $Q_{GR}$  (kcal/h)can roughly be correlated to the rate of oxygen uptake  $Q_{O_2}$  (millimoles of O2/h), since oxygen is the final electron acceptor.

$$Q_{GR} \cong 0.12Q_{O_2}$$

 Heat removal: by circulating cooling water through a cooling coil or cooling jacket in the fermentation.

## **Quantifying Growth Kinetics**

Monod equation: Unstructured Nonsegregated Model

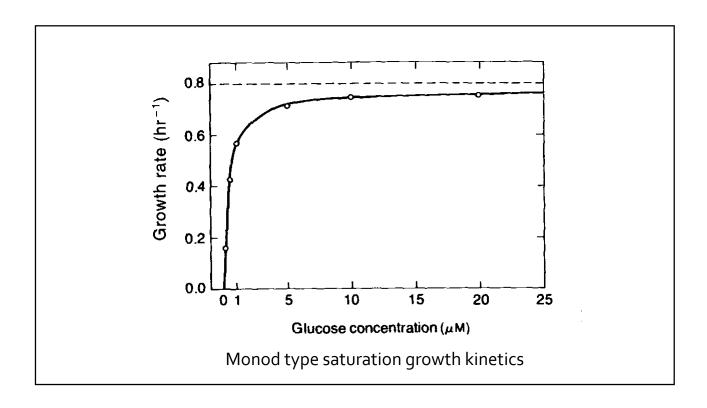
- Unstructured model: assuming <u>fixed cell composition</u>.
   Applicable to balanced-growth condition:
  - exponential growth phase in batch culture
  - single-stage, steady state continuous culture
  - cell response is fast compared to external changes
  - the magnitude of the external changes is not too large (e.g. 10% - 20% variation from initial conditions).
- Nonsegregated model: assuming all cells are the <u>same</u> in the culture.

## **Quantifying Growth Kinetics**

Monod equation: Unstructured Nonsegregated Model

### **Assumption:**

- a single enzyme system with Michaelis-Menten kinetics is responsible for uptake of substrate S, and the amount of that enzyme or its activity is sufficiently low to be growth-rate limiting.
- the relationship of specific growth rate to substrate concentration assumes the form of saturation kinetics.
- a single chemical species is growth-rate limiting while changes in other nutrient concentrations have no effect.



# Quantifying Growth Kinetics **Monod equation**

• When Monod equation is applied to cellular systems, the gross specific growth rate  $\mu_g$  (1/time) is described by:

$$\mu_g = \frac{\mu_m S}{K_S + S}$$

 $\mu_m$ : maximum specific growth rate (1/time).

 $K_S$ : saturation constant or half-velocity constant (g/l)

- If endogenous metabolism is unimportant,  $\mu_g = \mu_{net}$
- When the substrate concentration S>>  ${\rm K_S}$  (exponential growth phase),  $\mu_g=\mu_m$
- When the substrate concentration S<< K  $_{\rm S}$ ,  $\mu_g=(\mu_m/K_S)S$