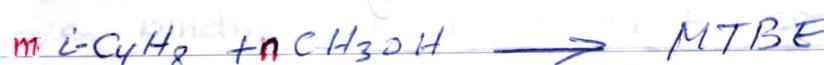


Catalysis & Catalytic Reactions

catalyst is a substance that affects the rate of Rxn by promoting different molecular paths (mechanisms) for Rxn, where this material does not change during Rxn.

Example: Methyl tert-butyl ether (MTBE) is produced by Rxn of isobutylene with methanol according



if this Rxn takes place on dodeca tungsto-salicic acid ($\text{H}_4\text{SiW}_{12}\text{O}_{40}$), HSiW then the rate of Rxn is

$$\begin{aligned} -r &= \frac{0.109 K_3 K_1}{k_2^{n-1}} P_{\text{C}_4\text{H}_8}^{1-n} P_{\text{CH}_3\text{OH}}^{1.76} \\ &= \beta P_{\text{C}_4\text{H}_8} P_{\text{CH}_3\text{OH}}^{2.76-n} \end{aligned}$$

However, if this Rxn takes place on the surface of MFI type zeolite, then the rate is

$$\begin{aligned} -r &= \frac{k_s k_a k_b}{K_{eq}} \frac{C_{\text{C}_4\text{H}_8}^a C_{\text{CH}_3\text{OH}}^b - C_{\text{MTBE}}^c}{(1 + k_a C_{\text{C}_4\text{H}_8} + k_b C_{\text{CH}_3\text{OH}} + k_c C_{\text{MTBE}})^{a+b}} \end{aligned}$$

Therefore, different catalyst yield different Rxn rates and different yield & selectivity of the product

Types of catalysis

1. solid catalyst's (heterogeneous) \rightarrow ~~in contact~~

2. liquid catalysts (homogeneous)

Example: salt water, oil (immiscible)

it is supported by such as transition metals on the surface of support, non supported, porous or molecular sieves

→ ~~immiscible~~ \rightarrow ~~solid~~ \rightarrow ~~liquid~~ \rightarrow ~~gas~~

characteristics of the catalysts

1. unchange during the Rxn

→ has large surface area w/ active site with specific activity

3. Rxn rate ↑ by decreasing activation energy

4. catalyst could change the selectivity of the Rxn

summary of catalytic Rxn steps

1. Transport of Rxnts from bulk to external surface

2. Diffusion of Rxnts from external surface into internal surface

3. Adsorption of Rxnts onto the internal surface

4. chemical Rxn on internal surface

5. Desorption of products from internal surface

6. Diffusion of product from internal to external surface

7. Transport of products into bulk.

special cases

A. Non porous catalyst (neglect 2 & 6)

B. Non porous + very quick adsorption & desorption (neglect 2, 6, 3 & 5)

Non porous + very rapid transport from / into bulk (neglect 2 & 6, 1, 7) $\Rightarrow A^*_{\text{part}} = (n + 1)^* A$

not dissociated

So what is Adsorption $A^*_{\text{part}} = A^*$

it is a binding of molecules to specific sites on a surface by either physical or chemical

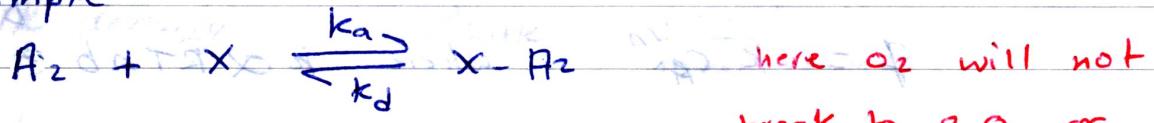
mean, ~~catalyst properties~~

Based on the binding type onto the surface of catalyst, adsorption can be classified as

1. undissociated (can not dissociate into

fragments, where the adsorbent (lattice) remain intact)

Example



$$r = k_a C_A C_{A^*} - k_d C_A^* \quad X-O_2 + X \cancel{\rightarrow} X-O + X-O-X$$

C_A : conc. of A in gaseous phase or liquid phase

C_{A^*} : = the vacant adsorption sites

C_A^* : conc. of the adsorbed A

$$\frac{C_A}{C_A + C_{A^*}} = x$$

@ equilibrium $r_{eq} = 0$, $k_a c_A c_U = k_d c_A^*$

$$\text{or } k_{eq} = \frac{k_a}{k_d}$$

$$c_A^* = k_{eq} c_A c_U$$

($c_T = c_U + c_A^*$)

But $c_U = c_T - c_A^*$; $c_T = \text{total surface area}$

$$\therefore c_A^* = k_{eq} c_A (c_T - c_A^*)$$

$$c_A^* (1 + k_{eq} c_A) = k_{eq} c_A c_T$$

$$\frac{c_A^*}{c_T} = \frac{k_{eq} c_A}{1 + k_{eq} c_A} = \frac{k_a c_A}{k_d + k_a c_A}$$

IN General $c_A^* = q_s = \frac{k_{eq} c_T c_A}{1 + k_{eq} c_A}$, $c_T = C_e$ monolayer

Langmuir model

what was the assumption

1. c_T is monolayer surface (not multi layer)

2. All surfaces have homogeneous energy (constant)

3. physical adsorption

How about if the surface has heterogeneous energy?

use empirical formula (Freundlich model)

$$\text{for this } q = K c_A^{1/n} \text{ where } K \propto RT^n b e^{-DH/RT}$$

X Shawabkeh & Tahirji proposed a model for chemical adsorption @ the surface of catalyst

$$q_t = q_s (1 - \alpha c_A)$$

$$\alpha = \frac{K \Delta t}{m_s q_s}$$