

Topic 3 : NPK fertilizer

* → straight fertilizers such as urea, single super phosphate (SSP), triple super phosphate (TSP), monoammonium phosphate (MAP), di-ammonium phosphate (DAP) are well defined products made using well defined processes.

→ compound or complex fertilisers such as NPK are more difficult to define as there is an infinite number of N/P/K ratios and processes applied in their production are numerous.

* product Name NPK is followed by 3 numbers to indicate the percent of N, P_2O_5 , and K_2O which the product contains
ex: 24-6-12 indicates 24% N 6% P_2O_5 12% K_2O
phosphorus compounds potassium compounds

fertilizer contain magnesium, boron, sulphur, ... etc
So typical content of nutrients ($N + P_2O_5 + K_2O$) normally be in
the range of 40-60%

*** Grades with no P_2O_5 or no K_2O are also included in the NPK product range but normally named NP & NK Fertilizers

* NPK fertilizers can be produced in four, basically different ways:

different ways:

✓ ① Ammonium phosphate / ammonium nitrate based NPK fertilizers

✓ ② Nitrophosphate based NPK fertilizers (mixed acid route).

③ Nitrophosphate based NPK fertilizers (ODDA-route).

④ mechanical blending of single or multi effect components.

production processes

- ① Granulation with a pipe reactor system
- ② Drum granulation with ammoniation
- ③ mixed acid process with phosphate rock digestion

Granulation with a pipe reactor system

- * incorporates one or two pipe reactors;
one pipe reactor is fitted in the granulator and another may be used in the dryer.
- * phosphoric acid or a mixture of phosphoric and sulphuric acids is neutralised in the pipe reactors with gaseous or liquid ammonia; wider range of grades, including ammonium phosphate can be produced
- * ① Granulation and drying section
 - required solid raw materials such as KCl , ... are mixed and fed into granulator together with the recycle
 - the pipe reactor fitted in the granulator is designed to receive phosphoric acid, ... and all the other liquid feeds.
 - concentrated ammonium sulfate may be added directly into the granulator
 - granules obtained are dried in drying section using heated air stream
- ② screening, crushing, cooling and coating
 - dry granules are screened into 3 fractions
 - oversize is removed and returned via crusher together with the fines
 - then it cooled in classical cooling equipment such as a fluidized bed cooler or cooling drum
 - cooled product is fed into coating drum where surface coating is applied to prevent caking.
- ③ Gas scrubbing and dust removed
 - venturi scrubbers scrubbed Gases
 - efficiency cyclones re-dusted Gases

Drum Granulation with ammoniation

* process consists granulation loop using mainly solid raw materials
ammonium nitrate solution is fed to the granulator

* ① Granulation and drying

→ - solid raw materials are metered and fed into granulator together with the recycle.

- Ammonium nitrate solution sprayed into granulator and sulphuric acid may be fed.

→ the granules obtained are dried in a drying section using heated air stream.

② screening, crushing, cooling and coating

- dry granules are screened into 3 fractions
over size is removed and returned to the granulator via the crusher with fines.

- on spec fraction is cooled in classical cooling equipment such as fluidized bed cooler or cooling drum

③ gas scrubbing and dust removal

~~gases from~~

same as method ①

Mixed acid process with phosphate rock digestion

① phosphate rock digestion and ammoniation

- first step is digestion of phosphate rock with nitric acid resulting in a solution of phosphoric acid and calcium nitrate.
- other raw materials such as phosphoric, sulfuric acid and nitric acid are added after digestion which is exothermic process. acid slurry is ammoniated with gaseous ammonia and after neutralization other components are added.

② Granulation, drying, screening, crushing, cooling and coating

- * in principle, the dry section divided into granulation part, drying part, screening / crushing part, a cooling part and a coating part.
- * granulation can be performed by different equipment
drum
blunger

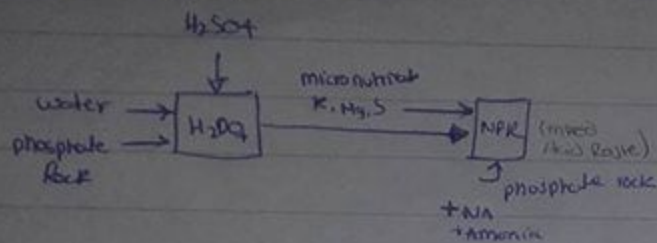
spherediser :

all granulation processes require drying operation after granulation
except the spherediser process

Local Industries

Best Available techniques for pollution prevention and Control in European Fertilizer industry

Production of phosphoric acid



Description of Production Processes:-

* Raw Material for phosphoric Acid

- Bones used to be the principle natural source - phosphorus.
- today it is produced from phosphatic ores mines.
- phosphate ores are 2 major geological groups:
 - 1. igneous $\rightarrow$ Kola, south Africa, Brazil
 - 2. sedimentary $\rightarrow$ Morocco, Jordan, Algeria, USA.

- the process is "thermal" when the raw material is elemental phosphorus.
- this process abandoned due to amount of energy needed
- wet process: that use phosphated minerals which are decomposed with an acid. This is the only economic way to produce phosphoric acid.

There are 3 subgroups of wet process:-

1. Nitric 2. hydrochloric 3. sulphuric $\checkmark$



There are 3 types of sulphuric Acid process, according to Calcium Sulfate Produced :-

1. anhydrite 2. hemihydrate 3. dihydrate.

Processes are the following:-

- 1- Dihydrate process
- 2- hemihydrate process
- 3- Di-hemihydrate process (soluble stage)
- 4- hemichy (Single)
- 5- " (soluble)

- different processes are needed due to different

1. Rocks + 2. gypsum disposal.

The storage and transfer of phosphoric acid is the same for all acids and doesn't depend on the method of production.

phosphate minerals in both types of ores are apatite group; the most encountered are

- fluoroapatite $\rightarrow$ igneous
- francolite $\rightarrow$ Sedimentary contain $(CO_3)_x$

* the most easily mined ores are in Sedimentation.

these sedimentary are connected to matter derived from organic compound (living creature) + waste + gangue minerals.

$\rightarrow$ Sedimentary phosphate ores have differing compositions within the same source.

* phosphate ores have to be concentrated or beneficiated before using/selling. different techniques are used in beneficiation. this gives rise to further variation in the finished ore concentrate product.

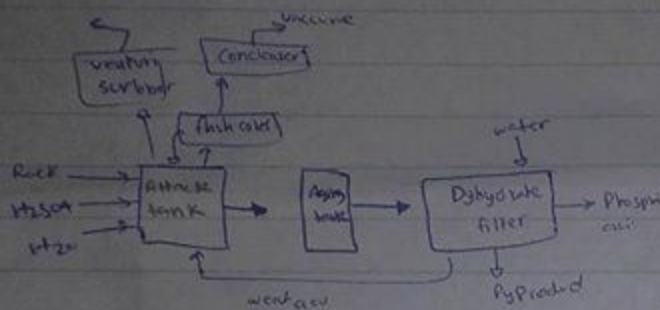
$\rightarrow$ rely on great material variety

The dihydrate stage are made of 4 stages.

1-grinding 2-reaction 3-concentration

3-filtration

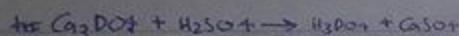
(Figure 3 page 15)



1-grinding

- ball/rod mill $\begin{cases} \text{wet} \\ \text{dry} \end{cases}$
- 60-70% $\rightarrow$ < 150 μm

2-Reaction



- in circulation.

- series of separated agitated reactors.

Can be replaced by single tank (economical)

can be separated by compartments.

- T = 70-80 26-32 P₂O₅

- cooler $\rightarrow$ delays the slurry $\rightarrow$ easier pumping.

3-filtration

1 ton P₂O₅ $\rightarrow$ 5 ton gypsum

separate phosphoric acid from CaSO₄

1-initial separation must be followed by

at least 2-stage washing? (efficiency)

Recover P₂O₅

- Pressure/vacuum Alternates
 $\downarrow$
Always used

Filtration equipments

1) tilting pan

2) rotary table

3) travelling belt

4) Concentration / direct contact concentration.

forced circulation: - HE

(figure 4)

- vapour/flash chamber
- condenser
- vacuum pump
- acid circulating pump
- circulation piping

2) Hemihydrate process (H.H.)

- CaSO₄ precipitated in hemihydrate

- produce 40-52% P₂O₅

- energy savings

- same previous stages but without grinding

Advantages:-

1) Reduction of evaporation heat requirements.

2) Capital Saving 3) Purer acid

$\rightarrow$ Acid from H.H. process tend to contain less free sulphur
 $\downarrow$ suspended solids $\downarrow$ Al, F

4) lower rock grinding required.

Disadvantages:

1) Filtration rate

H.H. crystals are small + less well formed than DH crystals.
thin clusters are harder to filter. this insures to use crystal habit modifier.

2) phosphate loss

3) filter cake impurities: more acid $\text{Ca} + \text{Cd} + \text{P}_2\text{O}_5$

4) Scaling

5) correction: $\leftarrow$ high high acid content.

+ recrystallization

1) HRC Acid $\rightarrow$ recrystallize $\rightarrow$ separate

2) 40-52% 2) HDH $\rightarrow$ separate $\rightarrow$ recrystallize $\rightarrow$ filter

3) 32-35 3) DH/HH Acid Dyn $\rightarrow$ separate $\rightarrow$ " $\rightarrow$ " $\rightarrow$ Return to liquor

- Rebulbing process:

further optimization of HRC process can be done

by re-slurrying and washing gypsum $\rightarrow$ 2nd filtration

So called Rebulbing.

Table 2: Advantages and disadvantages