



The University of Jordan

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Chemical Engineering Department

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Experiment Number (2)

Liquid-Liquid Equilibrium

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Abstract:

This experiment's goal is to explore liquid-liquid equilibrium when a solute (Acetone) is dissolved in a polar solution (water) and then transferred due to the difference in the chemical potential transferred to a second immiscible or partially immiscible organic non-polar solvent (Toluene). Cloudiness (turbidity) was the indicator of the three components being in equilibrium. The solvent that is enriched in solute is referred to as an extract, as is the solvent that is enriched in feed liquid and modest concentrations of solute. But in this experiment, the acetone is only partially dissolved by the raffinate and extract. The ternary phase diagram was plotted using the equilibrium points observed from different compositions for the solute and both solvents.

main Results



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Table of content

Abstract	2
Result	4
1.Ternary mutual solubility curve formation	on4
2.Tie Line determination	5
Discussion	8
Conclusion	9
D. C	10
References	11
Appendix	11
Table of tables	
Table (1): Densities at 20 °C in g/ml	4
Table (2): Water rich phase results	4
Table (3): Organic rich phase results	4
Table (4): Tie-Line determination data	5
Table (5): Tie-line composition and othmer-T	

Table of figures

Figure (1): Mutual solubility curve for ternary system of acetone, water, and toluene5
Figure (2): Ternary diagram of acetone, water, and toluene. Represent Tie-line6
Figure (3): Othmer-Tobias Correlation7
Figure (4): Wt % of Acetone in water saturated with Toluene Vs Refractive Index11
Figure (5): Wt % of Acetone in Toluene saturated with water Vs Refractive Index12

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Results:

Table (1): Densities at 20 °C in g/ml.

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Water density	Toluene density	Acetone density
0.9982	0.8669	0.7900

1-Ternary mutual solubility curve formation

A. For water rich phase

Table (2): Water rich phase results.

Water volume (ml) 20.00 20.00	Toluene volume (ml) 0.70	Acetone mass (g) 3.950	Water mass (g) 19.964	Toluene mass (g) 0.621	Total mass (g) 24.535	Acetone fraction (by mass)	Water fraction (by mass) 0.814	Toluene fraction (by mass)
(ml) 20.00	(ml) 0.70	(g) 3.950	(g)	(g)	(g)	(by mass)	(by mass)	(by mass)
20.00	0.70	3.950						
AL 1932	1					0.161	0.814	0.025
20.00	1.00							
	1.00	7.900	19.964	0.887 -	28.751	0.275	0.694	0.031
20.00	0.60	11.850	19.964	0.532	32.346	0.366	0.617	0.016
10.00	1.40	7.900	9.982	1.242	19.124	0.413	0.522	0.065
10.00	1.40	15.800	9.982	1.242	27.024	0.585	0.369	0.046
10.00	5.00	23.700	9.982	4.435	38.117	0.622	0.262	0.116
	10.00	10.00 1.40 10.00 1.40	10.00 1.40 7.900 10.00 1.40 15.800	10.00 1.40 7.900 9.982 10.00 1.40 15.800 9.982	10.00 1.40 7.900 9.982 1.242 10.00 1.40 15.800 9.982 1.242	10.00 1.40 7.900 9.982 1.242 19.124 10.00 1.40 15.800 9.982 1.242 27.024	10.00 1.40 7.900 9.982 1.242 19.124 0.413 10.00 1.40 15.800 9.982 1.242 27.024 0.585	10.00 1.40 7.900 9.982 1.242 19.124 0.413 0.522 10.00 1.40 15.800 9.982 1.242 27.024 0.585 0.369

B. For organic solvent rich phase

Table (3): Organic rich phase results.

Acetone	Toluene	Water	Acetone	Toluene	Water	Total	Acetone	Toluene	Water
volume	volume	volume	mass	mass	mass	i mass	fraction	fraction	fraction
(ml)	(ml)	(ml)	(g)	(g)	(g)	(g)	(by mass)	(by mass)	(by mass)
5.00	20.00	0.30	3.950	17.738	0.299	21.987	0.180	0.807	0.014
10.00	20.00	0.30	7.900	17.738	0.299	25.937	0.305	0.684	0.012
15.00	20.00	0.30	11.850	17.738	0.299	29.887	0.396	0.593	0.010
10.00	10.00	0.20	7.900	8.869	0.200	16.969	0.466	0.523	0.012
20.00	10.00	0.70	15.800	8.869	0.699	25.368	0.623	0.350	0.028
30.00	10.00	4.00	23.700	8.869	3.993	36.562	0.648	0.243	0.109

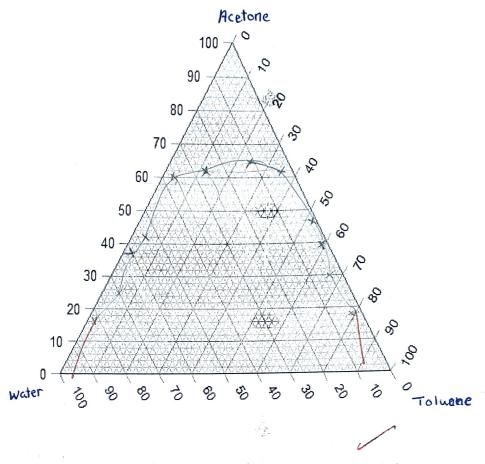


Figure (1): Mutual solubility curve for ternary system of acetone, water, and toluene.

2-Tie Line determination:

Table (4): Tie-Line determination data.

sample no.	water volume (ml)	Toluene volume (ml)	Acetone volume (ml)	water mass (g)	Toluene mass (g)	Acetone mass (g)	Total mass (g)	water mass fraction	Toluene mass fraction	Acetone mass fraction
1	18	20	13	17.968	17.338	10.270	45.576	0.394	0.380	0.225
	10	20	13	17.500	17.550	10.270	43.370	0.394	0.380	0.225
2	26	17	8	25.953	14.737	6.320	47.011	0.552	0.313	0.134
3	19	29	3	18.966	25.140	2.370	46.476	0.408	0.541	0.051

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Table (5): Tie-line composition and oth mer-Tobias Correlation

					and oth mer-To	bias Correlati	on.	
sample no.	RI of water layer	RI of toluene	Raff Mass	inate	Exti	act	othmer -Tobl	as correlation
		layer	fraction of acetone in water	Mass fraction of water in	Mass fraction of acetone in	Mass fraction of toluene in	log ((1-a)/a)	log ((1-b)/b)
1	1.3499	1.4709	layer 0.226	water layer 0.774	toluene layer 0.21	toluene layer 0.79	0.525	-
2	1.348	1.481	0.197	0.803	0.137	0.79	-0.535	-0.575 -0.799
3	1.3388	1.4893	0.05	0.95	0.075	0.925	-1.279	-1.091
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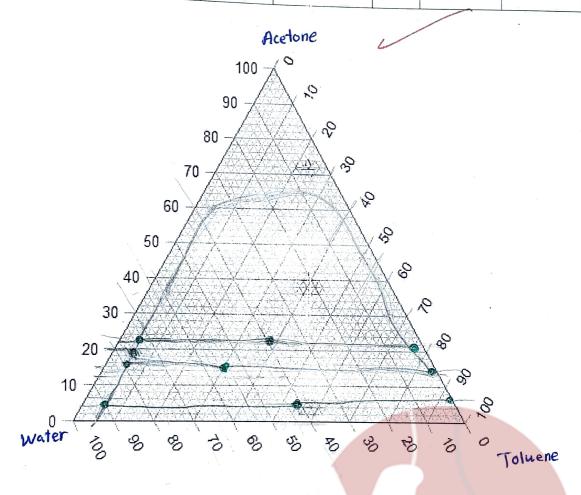


Figure (2): Ternary diagram of acetone, water, and toluene. Represent Tie-line.

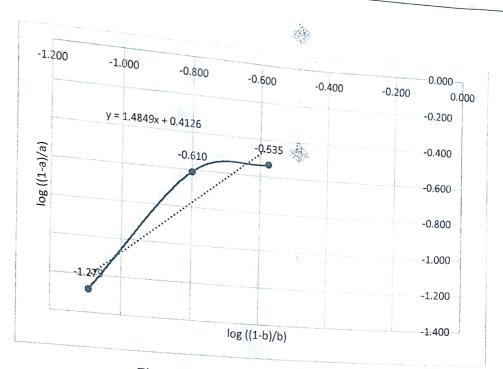


Figure (3): Othmer-Tobias Correlation.



Discussion

A phase diagram is a visual representation of a substance's physical states under various pressures, composition, and temperatures.

The main objective of using Phase diagrams is to illustrate the composition and the phase of a single or multiple component system. There are ternary diagrams, a sort of phase diagrams, which are triangular diagrams that depict the phase behavior of the three components of a combination under constant temperature and pressure. There are two varieties of ternary diagrams: equilateral triangles and the right triangle.

For this experiment, to represent all the equilibrium states between the extract and the raffinate layers after the separation process is carried out, ternary diagrams are used, an individual precise tie line is used to represent each state of equilibrium.

For a system made up of water, toluene, and acetone that is performed in a laboratory to gather the necessary experimental data, a ternary diagram is created. According to Table (2): Results for the water rich phase were obtained by taking six samples of the water rich phase and titrating them with toluene until cloudiness appears. This shows that the solution has changed from a one-phase to a two-phase region. The data is then plotted on a ternary diagram to create the water rich side of the solubility equilibrium curve. Comparatively, six samples of a solvent high in toluene were produced and titrated with water until turbidity was seen. The results are shown in Table (3). These findings were plotted to create the solvent side of the solubility equilibrium curve.

These two sides can be combined with a single line to generate a fully soluble line that divides the diagram into two regions: one phase and two phases. Figure (1): Acetone, water, and toluene ternary diagram, showing solubility equilibrium curve.

As you can clearly see, there is a variance in sample number six of the water-rich side (final row). This is a sign of an error, perhaps it is a personal error, that is in determining the cloudiness point or taking the correct reading from the burette.

The plait point should be determined, which is a point where the composition of the solventrich phase and the water-rich phase are equal, but it is challenging to identify due to sample

Using table (4): Tie-lines determination data lists the three samples, to generate the tie-lines. These samples represent a homogeneous mixture that, after settling in the cells, separated into two nonhomogeneous phases: water, acetone, and toluene, acetone. To determine the composition, the reflect index meter (RI) was used to evaluate the two phases.

As shown in Table (5): Tie-line composition and Othmer - Tobias Correlation. Three samples gave three tie-lines drown as best fit for the three points that is mentioned before which is shown in Figure (2): Ternary diagram of acetone, water, and toluene, represents Tie-lines.

Figure (3): Othmer - Tobias Correlation, to check for linearity where slope = 1.484 and

Conclusion

The experimental phase diagram is affected by personal errors, To identify the plait point, numerous samples must be taken. Cloudiness and turbidity both represent the observable change from a one phase mixture to a two phase mixture.

The physical states of a substance at various pressures, compositions, and temperatures are depicted in a phase diagram.

It is evident that sample number six from the side with more water differs from the others (final row). This is a sign that the cloudiness point was calculated incorrectly or the burette was properly interpreted—possibly a personal error.

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References

- 1- Manual Chemical Engineering Laboratory (2), Faculty of Engineering and Technology, Department of Chemical Engineering, The University of Jordan ,1/11/2022.
- 2- Seader, Henley and Roper, Separation Processes Principles -Chemical and Biochemical Operation, Chapter 4. John Wiley and Sons Inc., Third Edition ,1998.
- 3- Merck (2022). Pure Water Density Standard 1/11/2022 from https://macro.lsu.edu/howto/solvents/toluene.htm.
- 4- Toluene Solvent Properties , Acetone Solvent Properties https://www.sigmaaldrich.com/JO/en/product/sial/denwat1/11/2022.



Appendix

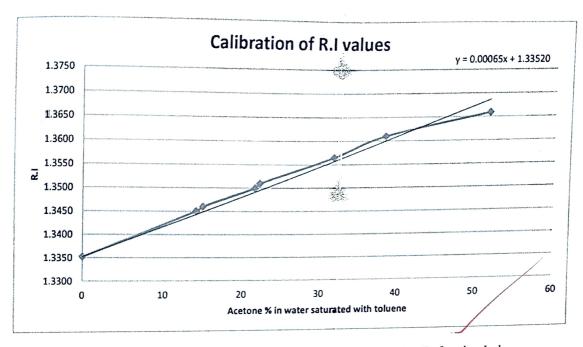


Figure (4): Wt % of Acetone in water saturated with Toluene Vs Refractive Index

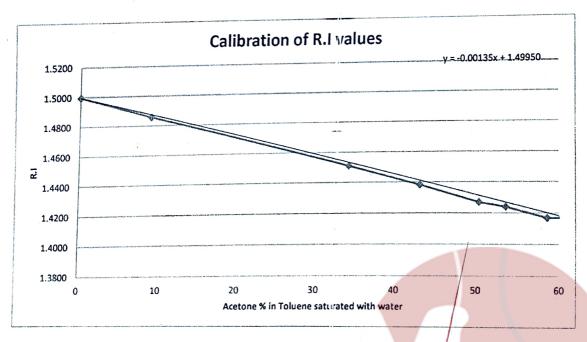


Figure (5): Wt % of Acetone in Toluene saturate d with water Vs Refractive Index

Sample of calculation:

(The calculations for the first row of each table will be shown)

❖ Mass = Density * Volume



- $Mass fraction = \frac{mass of component}{total mass}$
- ❖ Total mass = water mass + toluene mass +acetone mass

1. Ternary mutual solubility curve formation



1. For water rich phase (from table 2):

Volume of Water: 20.00 ml.

Density of Water at 20 °C: 0.9982 g/ml.

Mass of Water = 20.00 ml * 0.9982 $\frac{g}{ml}$ = 19.964 g.

Volume of Acetone: 5.00 ml.

Density of Acetone at 20 °C: 0.7900 g/ml.

Mass of Acetone = 5.00 ml *0.7900 $\frac{g}{ml}$ = 3.95 g.

Volume of Toluene: 0.70 ml.

Density of Toluene at 20 °C: 0.8669 g/ml.

Mass of Toluene = 0.70 ml * 0.8669 $\frac{g}{ml}$ = 0.607 g.

$$\underline{\text{Total mass}} = 19.964 \text{ g} + 3.95 \text{ g} + 0.607 \text{ g} = 24.521 \text{ g}.$$

Water mass fraction =
$$\frac{19.964 \text{ g}}{24.521 \text{ g}} = 0.814$$

Acetone mass fraction =
$$\frac{3.95 \text{ g}}{24.521 \text{ g}} = 0.161$$

Toluene mass fraction = $\frac{0.607 \text{ g}}{24.521 \text{ g}} = 0.248$

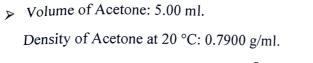
2. For Organic rich phase (from table 3):

Volume of Water: 0.30 ml.

Density of Water at 20 °C: 0.9982 g/ml.

Mass of Water = 0.30 ml * 0.9982 $\frac{g}{ml}$ = 0.299 g.





Mass of Acetone = 5.00 ml *0.7900
$$\frac{g}{ml}$$
 = 3.95 g.

> Volume of Toluene: 20.00 ml.

Density of Toluene at 20 °C: 0.8669 g/ml.

Mass of Toluene = 20.00 ml * 0.8669
$$\frac{g}{ml}$$
 = 17.338 g.

$$\underline{\text{Total mass}} = 0.299 \text{ g} + 3.95 \text{ g} + 17.338 \text{ g} = 21.58 \text{ i'} \text{ g}.$$

Water mass fraction =
$$\frac{0.299 \text{ g}}{21.587 \text{ g}} = 0.014$$

Acetone mass fraction =
$$\frac{3.95 \text{ g}}{21.587 \text{ g}} = 0.183$$

Toluene mass fraction =
$$\frac{17.338 \text{ g}}{21.587 \text{ g}} = 0.803$$

2. Tie-line determination:

A. Tie-line determination (from table 4):

> Volume of Water: 18.00 ml.

Density of Water at 20 °C: 0.9982 g/ml.

Mass of Water =
$$18.00 \text{ ml} * 0.9982 \frac{\text{g}}{\text{ml}} = 17.968 \text{ g}.$$

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> Volume of Acetone: 13.00 ml.

Density of Acetone at 20 °C: 0.7900 g/ml.

Mass of Acetone = 13.00 ml *0.7900
$$\frac{g}{ml}$$
 = 10.270 g.

> Volume of Toluene: 20.00 ml.

Density of Toluene at 20 °C: 0.8669 g/ml.

Mass of Toluene = 20.00 ml * 0.8669 $\frac{g}{ml}$ = 17.338 g.



$$\underline{\text{Total mass}} = 17.968 + 17.338 + 10.27 = 45.576 \text{ g}$$

Water mass fraction =
$$\frac{17.968 \text{ g}}{45.576 \text{ g}} = 0.394$$

Acetone mass fraction =
$$\frac{10.27 \text{ g}}{45.576 \text{ g}} = 0.225$$

Toluene mass fraction =
$$\frac{17.338 \text{ g}}{45.576 \text{ g}} = 0.380$$

B. Othmer - Tobias correlation (from table 5)

1. Finding (a) value:

RI of water layer =1.3499

From calibration curve of RI (values from figure (4)), the calibration equation y = 0.00065x + 1.33520

Mass fraction of acetone in water saturated with toluene, $x = \frac{(y-1.33520)}{0.065}$, applying this:

$$x = \frac{(1.3499 - 1.33520)}{0.065} = 0.226$$

Since we need to find the weight fraction of the solvent in the extract phase:

mass fraction of water in water layer = 1 - mass fraction of acetone = 1 - 0.226 = 0.774

2. Finding (b) value:

RI of toluene layer =1.4709

From calibration curve of RI (values from figure (5)), the calibration equation y = -0.00135x + 1.49950

Mass fraction of acetone in toluene saturated with water, $x = \frac{(y-1.4995)}{-0.135}$, applying this:

$$x = \frac{(1.4709 - 1.4995)}{-0.135} = 0.21$$

Since we need to find the weight fraction of the carrier liquid in the raffinate phase:

Mass fraction of toluene in toluene layer = 1 - mass fraction of acetone = 1 - 0.21 = 0.79

3. Checking reliability by Othmer - Tobias correlation

The reliability of equilibrium data for any system may be tested by applying the Othmer-Tobias correlation. This correlation states that:

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$$\log \frac{(1-a)}{a} = n \log \frac{(1-b)}{b} + s$$

there is a linear relation between the values of $(\log \frac{(1-a)}{b})$ and $(\log \frac{(1-b)}{b})$, where (a) represents water fraction in water layer, while (b) represents toluene fraction in toluene layer.

As sample of calculation, x, and f(x) can be found as below:

- $x = log(\frac{(1-b)}{b}) = log(\frac{(1-0.774)}{0.774}) = -0.535$
- $F(x) = log(\frac{(1-a)}{a}) = log(\frac{(1-0.79)}{0.79}) = -0.575$
- The same calculation has been applied on the other points and plotted to find the linear expression for the resulting line.

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Version no. 7 September, 2020

Liquid-Liquid Equilibrium Data Sheet

Tie-Lines Determination:

Volume of water (ml)	Volume of Toluene (ml)	Volume of Acetone (ml)	RI of water layer	RI of Toluene layer
20	15	15		1900
→ 18	20	13	1.3499	1.4709
→ 26	17	8	1.3480	1.4810
20	25	5		55.00
→ 19	29	3	1-3388	1.4893.

Solubility curve

A. Water rich phase:

Volume of Acetone (ml)	Volume of water (rnl)	Volume of Toluene (ml)
5	20 ete	0.70
10	20	1.00
15	20	0.60
10	10	1.40
20	10	1.40
30	10	5,00

B. Organic solvent rich phase:

Volume of Acetone (ml)	Volume of Toluene (ml)	Volume of water (ml)
5	20	ర ∙30
10	20	0.30
15	20	0.36
10	10	0,20
20	10	0.70
30	10	4:00

Instructor	signature:
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Date:

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